

## LIST OF SYMBOLS AND ABBREVIATIONS

In this book a naming convention is used in which (1) the number of characters required to identify a unique parameter is minimized and (2) the description of the parameter can be deduced in a logical way from its individual constituents. Thus in general a parameter is constructed from a combination of one or more main identifiers (either in capital- or in normal font) and one or more subscripts (both capital- and normal font).

The main identifiers indicate the class of the parameter, such as daily applied load or production (M), substrate (S), solids (X) or constants (K), while the subscripts specify the type involved, such as (<sub>v</sub>) = volatile, (<sub>t</sub>) = total, et cetera. Thus for example  $MS_{it}$  is defined as the total (<sub>t</sub>) daily applied mass (M) of organic material (S) in the influent (<sub>i</sub>).

In most cases a specific letter will therefore have more than one meaning. However, it is easy to deduct this from the context where it is used. As such the amount of characters required to uniquely identify a specific parameter is reduced to the minimum. In the remainder of this section the following lists will be presented:

- Common abbreviations;
- Specific parameters that fall outside the naming convention;
- Main classes (capital/normal font);
- Indices.

### List of common abbreviations

APT	= activated primary tank	PHB	= poly-hydroxy-butyrate
AT	= aeration tank	RWF	= rainwater flow
ATV	= abwasser technik verband	SSVI <sub>3,5</sub>	= stirred sludge volume index (determined at 3.5 g.l <sup>-1</sup> )
CIP	= cleaning in place	STORA	= stichting toegepast onderzoek naar de reiniging van afvalwater (Dutch foundation of applied water research)
CSTR	= completely mixed reactor	STOWA	= stichting toegepast onderzoek waterbeheer (Dutch foundation of applied water research)
DWF	= dry weather flow		
PF	= plug flow		
DSVI	= diluted sludge volume index		
EGSB	= expanded granular sludge bed	SVI	= sludge volume index
EPA	= environmental protection agency	TMP	= trans membrane pressure
GSBR	= granulated sludge bed reactor	TKN	= total Kjeldahl nitrogen
HUSB	= hydrolysis upflow sludge blanket	TOC	= total carbon concentration
MBR	= membrane bioreactor	TSS	= total suspended solids
OUR	= oxygen uptake rate	VFA	= volatile fatty acids
PAO	= phosphate accumulating organisms	VSS	= volatile suspended solids
		UCT	= university of Cape Town
		ZSV	= zone settling velocity

**List of parameters not included in naming convention**

a	= recirculation factor (-)
$a_{i,n}$	= annualisation factor (-)
$c_p$	= proportionality constant (DSVI/SSVI <sub>3,5</sub> )
$C_r$	= active sludge mass per unit daily applied biodegradable COD
$D_{C1}/D_{C3}$	= denitrification capacity in pre-D respectively post-D anoxic zone
f	= fraction remaining as endogenous residue
F/M	= feed/mass ratio (mg COD.mg <sup>-1</sup> VSS.d <sup>-1</sup> )
I	= investment costs (US\$)
i	= interest rate
k	= Vesilind constant (l.g <sup>-1</sup> TSS)
$k_{ia}$	= oxygen transfer coefficient (h <sup>-1</sup> )
$K_{1,2,3}$	= denitrification constant (mg N.mg <sup>-1</sup> X <sub>a</sub> .d <sup>-1</sup> )
$k_{1,2}$	= thermodynamic constants in the carbonic acid system
$K_a$	= adsorption rate constant (h <sup>-1</sup> )
$K_H$	= Henry constant (-)
$K_{mp}$	= specific utilisation rate of adsorbed organic material (mg COD.mg <sup>-1</sup> VSS.d <sup>-1</sup> )
$K_{ms}$	= specific utilisation rate of easily biodegradable organic material (mg COD.l <sup>-1</sup> )
$K_n$	= half saturation constant for nitrification (mg N.l <sup>-1</sup> )
$K_o$	= half saturation constant for oxygen (mg O <sub>2</sub> .l <sup>-1</sup> )
$K_{sp}$	= half rate (Monod) constant for $S_{pa}$ (mg COD.mg <sup>-1</sup> VSS)
$K_{ss}$	= half rate (Monod) constant for $S_{bs}$ (mg COD.l <sup>-1</sup> )
$k_w$	= dissociation constant for water
m	= gradient
n	= expected economical lifetime (years)
$p_m$	= energy dissipation per unit volume (W.m <sup>-3</sup> )
r	= anoxic recycle factor (bio-P system)
R	= annualised financing costs (US\$.year <sup>-1</sup> )
$R_{si}$	= minimum sludge age where $N_{av1} = D_{c1}$ (d)
$R_{sm}$	= minimum sludge age required to allow for anoxic zones, i.e. when $N_{ae} = N_{ad}$ (d)
$R_{sn}$	= minimum sludge age required for establishment of nitrification (d)
$R_{so}$	= minimum sludge age where $f_x = f_m$ (d)
$v_0$	= Vesilind constant (m.d <sup>-1</sup> )
u	= downward velocity in final settler (m.h <sup>-1</sup> )
v	= upward velocity in final settler (m.h <sup>-1</sup> )
v	= viscosity
$\alpha$	= alpha factor in aeration (-), gradient (m.m <sup>-1</sup> )
$\beta$	= beta factor in aeration (-)
$\theta$	= temperature dependency

**List of main parameters**

A	= area
Alk	= alkalinity
B	= recovery factor
b	= decay rate
C	= cost per unit measure
C	= concentration
D	= diameter
DO	= dissolved oxygen concentration
E	= excess sludge production
F	= mass flux
f	= fraction, mass fraction or ratio
H	= unit depth/height
h	= liquid depth/height
I	= index
k, K	= constant
M	= system mass, daily load or production (generic)
m	= mass per unit daily applied influent COD effluent
mw	= molar weight (generic)
N	= nitrogen
N	= number
O	= oxygen demand
OC	= oxygenation capacity
P	= phosphorus
P	= power or energy dissipation
p	= pressure
Q	= influent flow rate
q	= excess sludge flow rate
R	= residence time
R	= removal efficiency
r	= reaction rate
S	= organic substrate
s	= sludge recycle factor
s <sub>f</sub>	= safety factor
T	= temperature
T	= hydraulic loading rate
V	= volume
X	= solids
Y	= yield
η	= efficiency, productivity
μ	= growth rate

**List of indices**

a	= ammonium/ammonia (N)
a	= active sludge (X)
a	= actual conditions (OC, DO)
a	= adsorption/storage (S, r)

abs	= absorption (OUR, k)
ac	= additional cost (f)
ad	= desired concentration (N, P)
ad	= adiabatic compression (P, η)
ae	= aerator (η)
air	= air (Q)
am	= ammonification (Alk)
an	= ammon. oxidation (Y, b, K, μ)
an	= anaerobic (f, Y, b)
an	= anoxic sludge mass fraction (f)
ao	= ammonium oxidizer (Y, b, K, μ)
ap	= active sludge bio-P (X)
ap	= apparent (Y)
at	= ratio active/total sludge (f)
av	= available nitrate (N)
av	= average (F, Q, X)
av	= ratio active/volatile sludge (f)
b	= biodegradable (f, S)
b	= buffer (X, V, H, h)
BOD	= biological oxygen demand (k)
c	= capacity (D, N)
c	= conversion to VFA (k)
c	= critical (s, X)
c	= fermentation (K)
c	= oxidation of org. material (O)
chem	= chemical removal (P)
cv	= ratio COD/VSS (f)
d	= decay (r)
d	= denitrified (Alk, N)
d	= digested (S, N, P)
d	= divalent ion (f)
d	= drying (T)
d	= final settler (A, V, H, C)
da	= aerobic digester (V, R)
di	= anaerobic digester (V, R, C)
dif	= diffusor height (H)
dis	= discharge (p)
diss	= dissipated (P, p)
dl	= discharge levies (C)
dn	= denitrification (f)
dsv	= diluted sludge volume index (I)
Ds	= nitrate removal with S <sub>bs</sub> (N, r)
Dp	= nitrate removal with S <sub>bp</sub> (N, r)
e	= effluent (dissolved) (X, S, N, P)
e	= endogenous residue (X)
e	= excess sludge production (r)
el	= electrical (P, η), electrons (N)
en	= endogenous (O)
ep	= endogenous bio-P (X)
eq	= equivalent (O, N)

ex	= exogenous (O)	p	= particulate (S)
g	= gross (F)	p	= bio-P organism (b, f, X)
g	= growth (X, r)	p	= primary sludge (E,X)
h	= heating (C)	p	= nitrification potential (N)
h	= heterotropic (b, Y, X)	p	= permeate (Q)
h	= hydraulic (R, OUR)	p	= personnel (I)
H	= Henry	p	= phosphate (P)
hi	= hydrolysed/hydrolysis (r)	p	= phosphorus (f)
i	= inert (X, S)	p	= pressure (DO)
i	= influent (Q, S, N, P)	pd	= denitrifying fraction (f)
i	= investment (f)	pf	= peak flow (Q, f)
inh	= inhabitant (V, S)	pr	= phosphate release (f)
k	= Kjeldahl (N)	pu	= putrescible (f)
k	= in reactor "k"	r	= reactor (aeration tank) (V, C)
l	= demand for excess sludge (N, P)	r	= recycle (Q, X)
l	= in mixed liquor (DO)	rc	= recirculation (Q, X)
l	= limiting (F, X)	ref	= reference conditions (P)
liq	= liquid height (h)	s	= saturation (DO)
le	= demand in stabiliz. sludge (N, P)	s	= soluble (S, f)
lex	= demand for excess sludge, corrected for effluent loss (N, P)	s	= sludge age (R)
m	= maintenance (I)	s	= standard conditions (OC, DO, p)
m	= maximum (f)	s	= superficial (T)
m	= membranes (A)	sd	= sludge disposal (C)
m	= minimum (X, F)	sol	= solids loading (F)
m	= monovalent ion (f)	seq	= sequestered (S)
m	= motor (P)	spec	= specific (A)
max	= maximum (f)	ssv	= stirred volume index (I)
mb	= metabolised (S)	t	= temperature
Me	= metal salt (M)	t	= total
me	= methane (V)	te	= total effluent (S, N, P)
min	= minimum (C)	th	= thickened (X)
mod	= module (A, V)	th	= thickener (V, A)
N	= N <sup>th</sup> reactor	u	= recycle sludge abstraction (F)
n	= insurance (I)	u	= utilized/utilization (r)
n	= net (F)	u	= UASB (C, R, S, V)
n	= nitrate (N)	v	= volatile (f, X)
n	= nitrification (Alk, O)	v	= settling velocity (F)
n	= nitrifiers (N, P, X, Y, b)	vfa	= volatile fatty acids (S)
n	= nitrogen (f)	vx	= sludge volume (T)
n	= nitrogenous material (B)	w	= water vapour (p)
n	= non biodegradable (f, S)	x	= sludge mass fraction (f)
no	= nitrate oxidizers (b, K, $\mu$ )	xa	= active sludge
no <sub>2</sub>	= nitrite (N, r)	xv	= volatile sludge
nxa	= inactive sludge	0, 1	= initial; primary or pre
o	= operational (I)	2, 3	= secondary, tertiary or post
o	= nitrogen (N)	20	= 20°C
o	= oxidized (S, r)	$\infty$	= infinity (for limits)
O <sub>2</sub>	= aeration (C), oxygen (P)		
p	= particle (K)		

